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Mediating the Catalytic Selectivity of Au Nanoclusters by Ligand Engineering

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Abstract: It was well-established that the thiolate ligands laid significant influence on the catalytic properties of protected Au nanoclusters (NCs for short), especially the selectivity. In this work, catalytic nitro reduction is investigated over nanocluster catalyst. The electron-withdrawing property of thiolates renders the surface positively charged, which results in less aniline derivatives. The conversion is found to augment a lot after complete removal of capping thiolates, owing to the accessibility of active sites on Au NCs. Furthermore, a range of functionalized substrates are investigated for the universality of this catalytic reaction, and the composite catalysts show good tolerance to functional groups. Moreover, the exterior ligands were gradually peeled off by thermal treatment through controlling the temperature under vacuum, and the as-prepared catalysts were characterized by TEM, FTIR measurements. Using these catalysts, the relationship between the extent of ligand removal and the catalytic activity/selectivity was investigated.

Key words: ligand effect; selectivity; Au nanoclusters; nanocatalysis

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Recently, gold nanoclusters (NCs for short) have gained popularity for their catalytic properties owing to the quantum effect and high volume/surface ratio^[1]. Among them, NCs with ultra-small size (less than 2 nm with metallic kernel) glint the most because of high surface-to-volume ratio, the surface geometric effect the electronic effect, as well as the quantum size effect^[2-3]. Additionally, the atomically precise NCs pose the potential for fully understanding the structure-property correlations owing to their exact structure^[4-6]. By investigating the size effect on catalytic activity, it has been proved that clusters with size at about 2 nm exhibit the best performance^[7-9]. Besides the size dependence, previous literature paid tremendous attention to the expansion of reaction type^[10-14], better activity^[15-16], synergistic effect^[17-20], and mechanism research^[21-23].

The ligands bonded on the surface of gold NCs block the contact between substrate and gold, which results in low conversion in catalysis; however, organic ligands could also modulate the electronic states of

NCs^[24-26]. Additionally, the electronic states have a major influence on the catalytic conversion, but also the product selectivity^[27-33]. Li *et al.* unravelled that the species of capping agents could tune the electronic and catalytic properties of Au NCs theoretically and experimentally^[34]. Xie *et al.* elucidated the catalytic performance of NCs could be interfered by the length of S ligands and functional moiety^[35]. Obviously, the capping ligand is a significant parameter affecting the catalyst activity, and the management of ligand could hopefully be an efficient way to design better catalyst with enhanced performance. The thiols are the most popular ligands in the synthesis of Au NCs^[36-39] since the Au-S bond is much stronger than any others, correspondingly, they affect the performance of Au NCs catalyst quite dramatically.

In this paper Au₂₅L₁₈ (L = PhC₂H₄S) was employed as a model catalyst to evaluate the influence of capping agent on the catalytic activity and selectivity. The reduction of nitrobenzene usually gives rise to phe-

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nylhydroxylamine, aniline, azobenzene, azoxybenzene and hydrazobenzene as products. Hence, it is introduced as a probe reaction. The capping ligands were gradually removed by increasing the incineration temperature step by step. As the NCs readily aggregate under high temperatures, the heterogeneous support thus becomes indispensable for preventing aggregation. Porous structured nickel silicates are used as the support; their high surface area of $280 \text{ m}^2/\text{g}$ efficiently inhibits aggregation of NCs, and the chemically inert character rules out their interference to the investigation of ligand effect.

The nickel silicates and Au_{25} NCs were synthesized according to the previous literature^[40–41]. The immobilization of Au NCs was accomplished by means of adsorption and calcination. After collecting the deposit of centrifuged solution, the $\text{Au}_{25}/\text{Ni-SiO}_2$ composite was dried under vacuum at 50°C . By increasing the incineration temperature, which was 150, 200, 250 and 300°C step by step, partial to complete S ligand removal was achieved. Heating for 2 h at 300°C was enough to completely peel off the capping agents based on the TGA analysis^[26], avoiding severe aggregation of NCs. All the ligands were untouched if the composite hadn't been subject to the heat treatment. The unprocessed composite catalysts were introduced as the basis for comparison. Hereafter, the composite catalysts treated at different temperatures were referred as $\text{Au}_{25}@\text{Ni-SiO}_2(\text{RT})$, referring to room temperature, which was not processed by heating), $\text{Au}_{25}@\text{Ni-SiO}_2(150)$, $\text{Au}_{25}@\text{Ni-SiO}_2(200)$, $\text{Au}_{25}@\text{Ni-SiO}_2(250)$ and $\text{Au}_{25}@\text{Ni-SiO}_2(300)$, respectively.

1 Experiments and characterization

All the chemicals and reagents are purchased from Aladdin Corporation with GR grade. TLC plates (Merck Silica Gel 60 F254) were used for analytical TLC, and Merck Kieselgel 200~300 was used for preparative column chromatography. Conversion and selectivity were measured with Shimadzu (Japan) GC 2010 plus. TEM images were obtained by JEM 2100 (Japan). The intermediates and product identification was carried out by Saturn2200 GC-MS of Varian (America). The sam-

ples were weighed with a Mettler Toledo MX5 scale with $d=0.1 \text{ ug}$ (Swiss). IR spectra were recorded with Bruker Hyperion Vertex80 (German) by using KBr carrier. The quantification of Au content of the composite catalysts was assessed by ICP AES (Inductively Coupled Plasma Atomic Emission Spectrometer) of I-RIS intrepid II XSP which is purchased from Thermo Electron (America). The specific surface area of samples was obtained based on an N_2 adsorption-desorption isothermal analysis (V-Sorb 2800P, Gold APP Instruments, China) with the Brunauer-Emmett-Teller (BET) model.

The synthesis of $\text{Au}_{25}(\text{SCH}_2\text{CH}_2\text{Ph})_{18}\text{-TOA}^+$ (TOA = tetraoctylammonium bromide) and porous nickel silicates were described in previous literature. After both were prepared, 5 mg Au_{25} (dissolved in a spot of THF, short for tetramethylene oxide) was added into 100 mL ethanol along with 650 mg silicates. The mixture was sonicated for 10 minutes, followed by stirring for 2 h. Afterwards, the mixture was centrifuged to remove unabsorbed NCs, and the sediment was dried under vacuum at 50°C . The different catalysts were treated at 150, 200, 250 and 300°C for 2 h. The calcination program was set as room temperature heating up to 50°C for 30 min, preserving for another 30 min before taking 2 h heating up to 150°C , and finally preserving for 2 h before cooling down. A round bottomed flask was charged with 0.2 mL (2 mmol) nitrobenzene and 0.112 g NaBH_4 (4 mmol), 30 mg immobilized catalyst ($\text{Au } 6.1\times 10^{-3} \text{ mmol}$), and 2 mL EtOH/2 mL H_2O . After stirring at 90°C under vacuum for 2 hours, the reaction was completed. The product was analyzed by GC-MS.

2 Results and discussion

The immobilization of Au NCs was accomplished by blending the support and NCs in ethanol, then drying the sediments after collecting them. All the supported catalysts were prepared in the same batch to unify the Au loading, but treated at different temperatures to control the different degree of ligand desorption. The Au loading was determined by ICP-AES tests to be 0.4% wt. The BET surface of as-prepared Ni-

SiO_2 sphere is $280 \text{ m}^2 \cdot \text{g}^{-1}$, which is higher than amorphous material.

The unheated $\text{Au}_{25}@\text{Ni-SiO}_2$ composite and other

catalysts calcined at 150, 200, 250 and 300 $^\circ\text{C}$ were all characterized by HRTEM to determine the size distribution after immobilization and heat treatment (Fig.1).

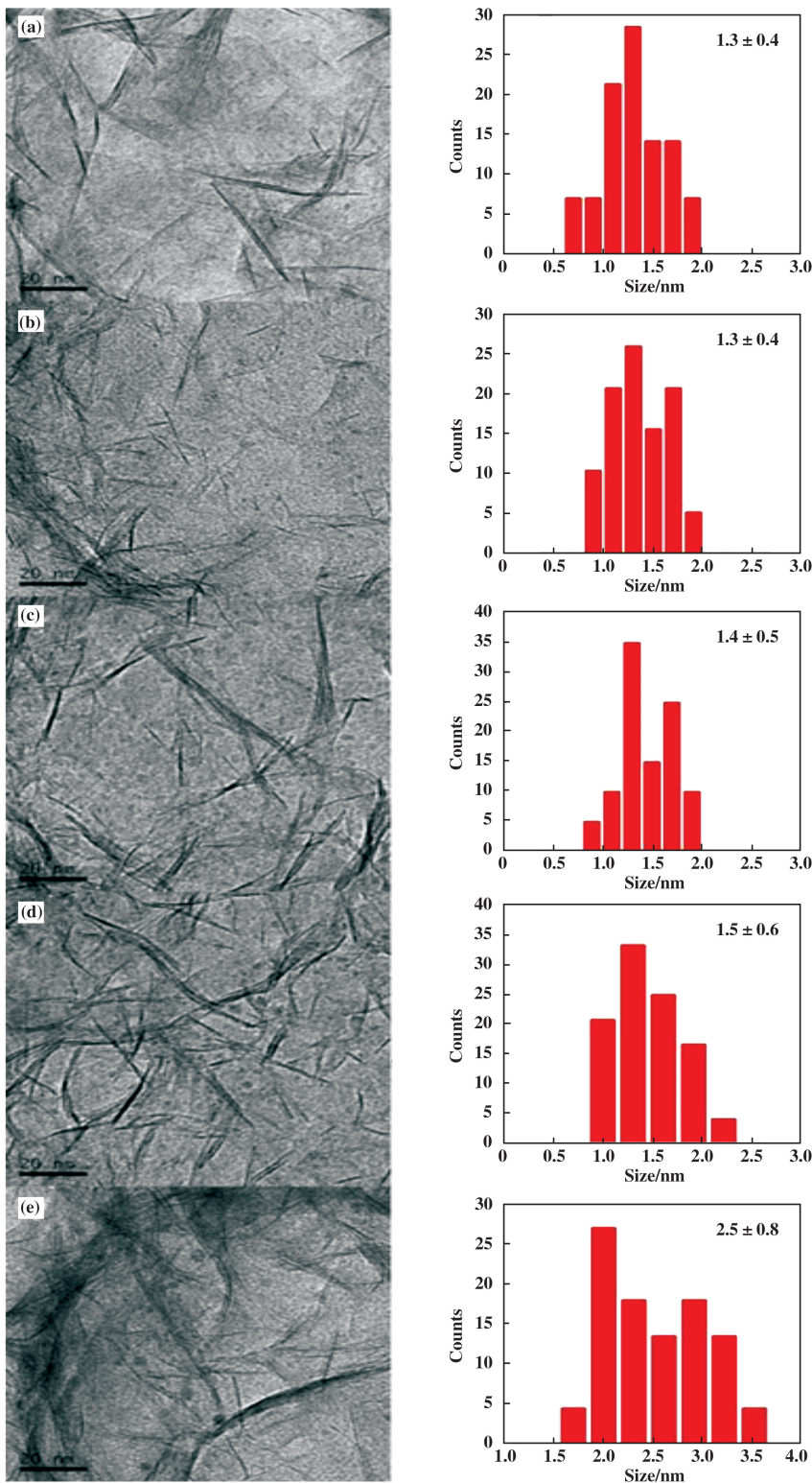


Fig.1 TEM images and size histograms of NCs supported on porous Ni-SiO_2 spheres, the scale bar is 20 nm in each panel

The calcination temperature is none (a), 150 $^\circ\text{C}$ (b), 200 $^\circ\text{C}$ (c), 250 $^\circ\text{C}$ (d), 300 $^\circ\text{C}$ (e), respectively

The average size of Au₂₅@ Ni-SiO₂(RT) is 1.3 nm, indicating that the immobilization procedure didn't lead to the aggregation of Au₂₅(Fig. 1a).

TGA analysis showed no ligand loss under 170 °C, thus the structure of Au₂₅ should not collapse given that the Au₂₅(SR)₁₈ structure is the most thermodynamically stable one. The 150 °C-treated Au₂₅@ Ni-SiO₂ did not show any observable size enhancement (Fig.1b). However, the composite heated at higher temperature led to slight aggregation; the average sizes were larger, and the size distribution was broadened;

1.4±0.5 nm for 200 °C and 1.5±0.6 nm for 250 °C; when the heating temperature was increased to 300 °C, the size increased further (2.5±0.8 nm) larger than the starting one (1.3 nm±0.4 nm). The high temperature was required to stripe off the capping ligands from the surface of Au NCs; slight aggregation was the cost. Fortunately, the size alteration was negligible, thus it is still reliable to conclude the relationship between catalytic property and ligand effect.

FTIR was employed to detect the residue ofthiolate ligand (Fig.2). Since the Au loading was as low as

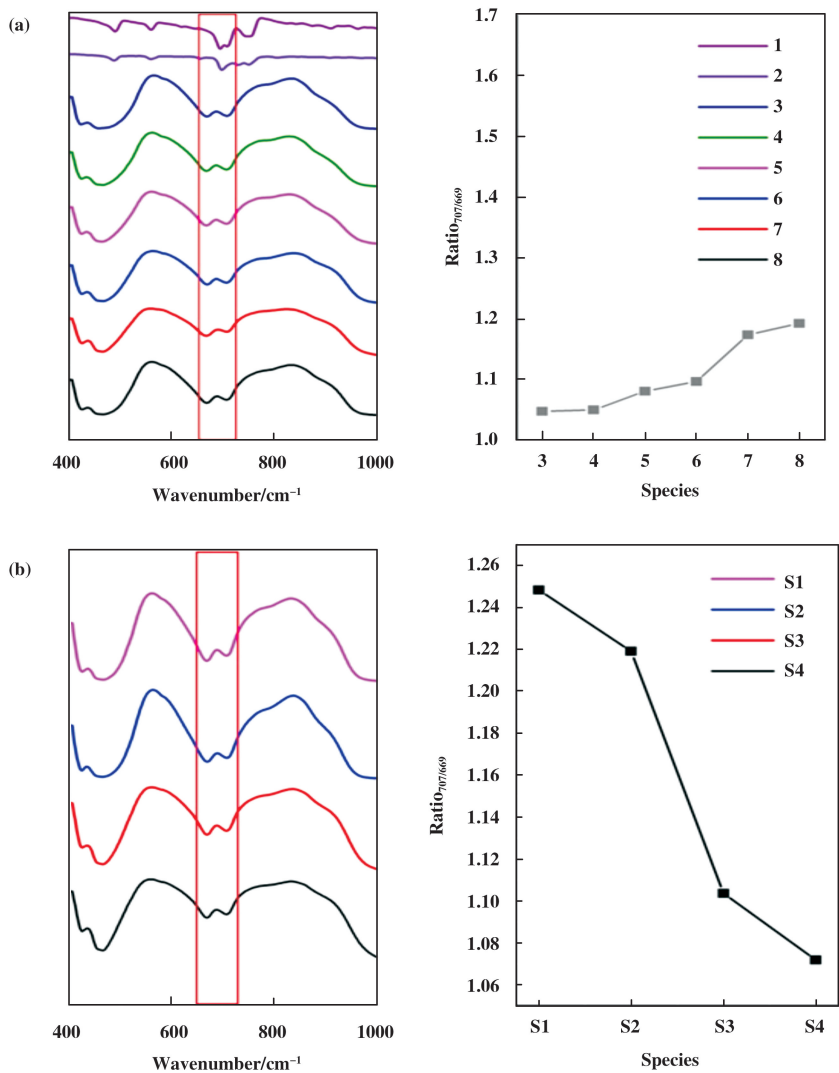


Fig.2 (a) FTIR spectra of Au₂₅, Ni-SiO₂ and supported catalysts calcined at different temperature (left) and ratio of transmission between 707 cm⁻¹ and 669 cm⁻¹(right) ; 1-8 stand for PhCH₂CH₂SH, Au₂₅, Au₂₅@ Ni-SiO₂(RT), Au₂₅@ Ni-SiO₂(150), Au₂₅@ Ni-SiO₂(200), Au₂₅@ Ni-SiO₂(250), Au₂₅@ Ni-SiO₂(300), Ni-SiO₂, respectively. (b) FTIR spectra of pure Ni-SiO₂ calcined at different temperature (S1-150 °C, S2-200 °C, S3-250 °C, S4-300 °C) and ratio of transmission between 707 and 669 cm⁻¹

0.4% wt, and the ligand content in the NCs was only 37%, IR was a better method to distinguish the organic remaining than using other conventional instruments. The typical IR adsorption peak of mono-substituted benzene ring is at 694 cm^{-1} , while it shifts to 700 cm^{-1} when the $\text{PhC}_2\text{H}_4\text{S}$ was bonded to the Au NCs, and further shifts to 707 cm^{-1} when the NCs are immobilized on the Ni-SiO₂ spheres. The adsorption band centered at 669 cm^{-1} is assigned to the intrinsic sphere support. However, another adsorption band centered at 707 cm^{-1} was overlapped with the organic component, as a result, the two peaks merged into a bigger one. It is thus not possible to quantify the exact amount of S residue of all the catalysts, considering the film thickness of IR samples being difficult to consolidate. Fortunately, the ratio between 707 and 669 cm^{-1} could be utilized as an efficient tool to represent the concentration of S remaining in the composite catalysts, because the transmission at 669 cm^{-1} is always linear with the sample content. As shown in Fig.2a, the 707 cm^{-1} peak continually became weaker along with the increasing calcination temperature (left). The plot on the right panel gave more intuitive result: no ligand loss between $150\text{ }^\circ\text{C}$ and room temperature; and then gradual loss was observed when the temperature was further augmented. The structure should collapse in the $300\text{ }^\circ\text{C}$ treatment for 2 h, which was verified by TGA and TEM images, and the organic capping agents were totally stripped off from the Au surface. Since the Ni-SiO₂ supports were also incinerated under the same circumstance, the factor had to be taken into account (see Fig.2b). However, it was observed the transmission ratio between 707 and 669 cm^{-1} decreased in responding to gradually increased heating temperature, which was quite opposite to the Au@ Ni-SiO₂ case. The outcome further suggests the gradual loss of capping ligands.

Hydrogenation of nitrobenzene was investigated as a model reaction to evaluate the ligand effect on the catalytic properties. The products generally include aniline (referred to AN), azobenzene (AZO) and azoxybenzene (AXY). Control experiments were performed to confirm the catalytically active component. The extreme condition of $90\text{ }^\circ\text{C}$ (with no catalyst) gave rise to

a little conversion and the product was completely AXY (Fig.3, item 0), and pure Au₂₅ gave a little higher

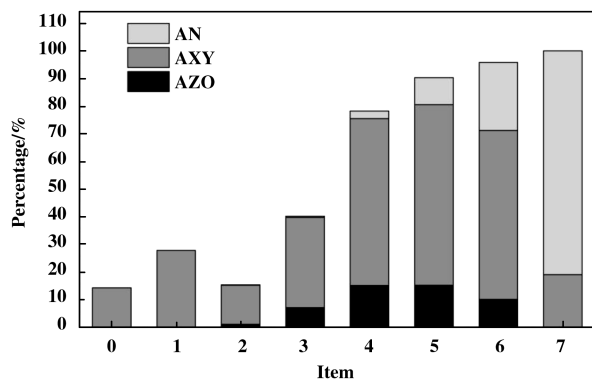


Fig.3 Conversion and selectivity of nitrobenzene catalyzed by all kinds of catalysts. 0 ~ 7 stand respectively for blank, Au₂₅, Ni-SiO₂, Au₂₅ @ Ni-SiO₂ (RT), Au₂₅ @ Ni-SiO₂ (150), Au₂₅ @ Ni-SiO₂ (200), Au₂₅ @ Ni-SiO₂ (250), Au₂₅ @ Ni-SiO₂ (300). The height of the whole bar is the conversion percentage, the ratio between individual bars of different color is the selectivity

than that (item 1). Ultra-small NCs were readily aggregated under these circumstances, which resulted in poor activity. The item 2 ruled out the support as the active component, thus it acts as an essentially inert support in our system. The Ni-SiO₂ support was supposed to protect the NCs from detaching and aggregating. However, without the annealing process, the physically adsorbed NCs could not avoid the activity drop (item 3). Simultaneously, more AZO was generated and AN emerged. After annealing at $150\text{ }^\circ\text{C}$, the supported catalysts gave rise to a conversion jump while more AN and AZO were observed. Along with the increasing sintering temperature, the conversion exhibited a linear enhancement, and the selectivity preference exhibited an upside down shift: AZO decreased to none and the primary product turned into AN.

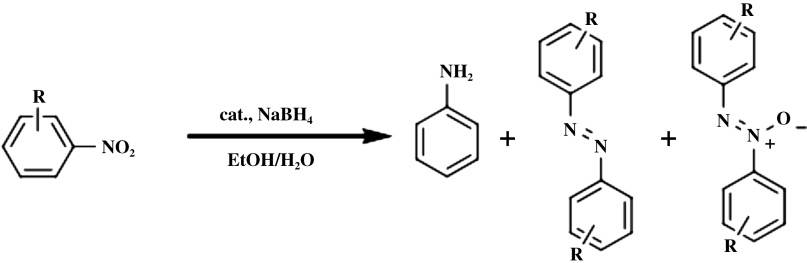
After high temperature calcination, the Au₂₅ NCs were not themselves anymore. Given that the NC size didn't display severe aggregation, it was still reasonable to conclude the relationship between catalytic performance and ligands concentration. The external organic agents more or less block active sites and thus lead to low catalytic activity. Correspondingly, the re-

removal of capping ligands releases some power on catalysis. More importantly, the ligand influence on the product selectivity became dazzling. There are two possible effects of the residual thiolates on the catalysis: steric and electronic effects^[17]. Nevertheless, the steric hindrance of aniline was weak, while it was the primary product when all the capping agents were removed, suggesting that the steric effect was not the cause of the observed results. Au₂₅ NCs with residual thiolates are more positively charged than the naked

Au₂₅ (i.e. essentially zero valence) owing to electron withdrawing by the S atoms, that's why the more reduced product aniline dominates in the products. Interestingly, the preference of AZO generated a down-para-curve pattern; it might be because of the more open catalyst surface and the more positively charged property.

The as-prepared catalysts were tested for functional group tolerance (Table 1). Only the two opposite catalysts, Au₂₅@Ni-SiO₂(150) and Au₂₅@Ni-SiO₂(300)

Table 1 Hydrogenation of nitrobenzene derivatives catalyzed by Au₂₅@Ni-SiO₂(150) and Au₂₅@Ni-SiO₂(300)^[a]



Entry	Substrate	Calcination Temperature /°C	Reaction Temperature /°C	Time /h	Conversion /%	Selectivity/%		
						Aniline	Azo	Axy
1		150	RT	8	21.2	15.4	19.2	65.4
		300			100	75.9	0	0
2		150	100	2	98.1	0	81.9	18.1
		300			100	65.7	11.9	22.4
3		150	100	2	1.5	0	58.6	41.4
		300			100	50.8	24.9	24.3
4		150	RT	8	0.6	69.3	30.7	0
		300			98.7	98.8	1.2	0

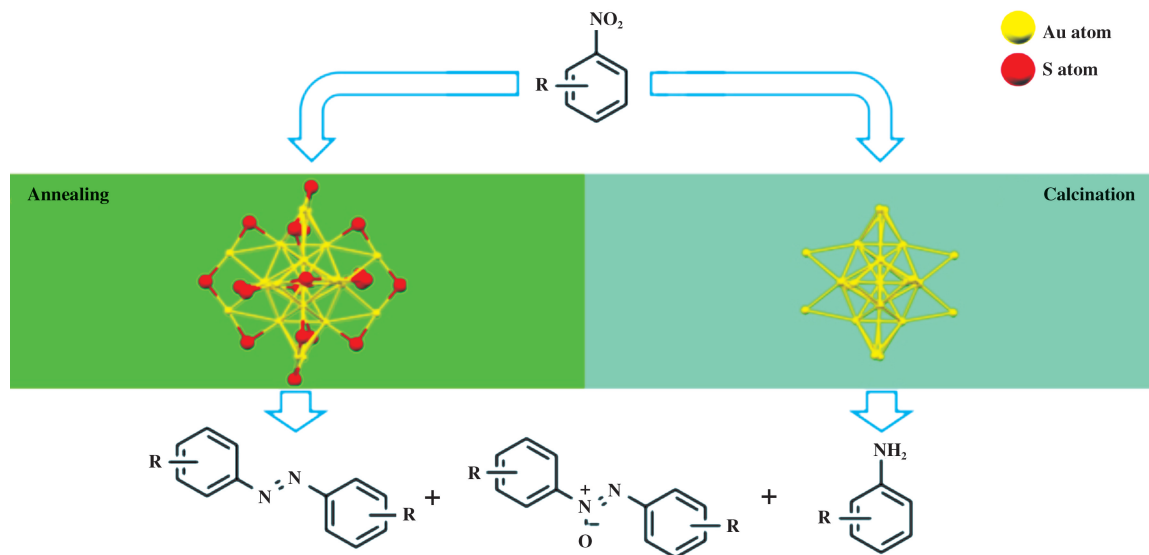
a. Reaction condition: 2 mmol substrate, 4 mmol NaBH₄, 30 mg immobilized catalyst (Au 6.1 × 10⁻³ mmol), and 2 mL ethanol/ 2 mL H₂O

(300), were compared, as they gave the sharpest contrast. It was observed that derivatives with electron-withdrawing groups (entries 1, 4) were more active than those with electron-donating groups (entries 2 and 3), since the room temperature was enough to convert

the substrates over the catalysts. The results were consistent with previous patterns though some byproducts were generated. The Au₂₅@Ni-SiO₂(150) composite with S component gave rise to AXY derivatives as dominant products, while the other competitor yielded

overwhelmed anilines. The steric effect from substrates was considerable as well. The groups on the para-positions didn't interfere the contact between substrates and catalysts, and gave excellent conversion (entries 2). On the contrary, the groups on the ortho-position hindered the access to metal (entries 3 and 4), along with the exterior ligands of $\text{Au}_{25}@\text{Ni-SiO}_2(150)$ bloc-

king the substrate approaching the active sites, hence low conversion at ambient conditions. As a result, the conversion was too low to make big differences on the product preference. These systematic results comprehensively verified the ligand effect on the catalytic properties, including activity and selectivity as scheme 1 illustrated.



Scheme 1 Illustration of selective benzylamine reduction by protected and naked gold NCs

3 Conclusions

This work reveals that the exterior ligands of Au NCs have a great influence on the catalytic properties, in particular on the product selectivity. The electron-withdrawing property of thiolates makes the NCs positively charged, and the removal of the ligands restores the neutral valence state. Overall, our experimental results shed light on the catalytic mechanism by using atomically precise gold NCs, which offers some clues for designing more efficient catalysts.

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选择性控制的配体工程在金团簇催化中的作用

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摘要: 金团簇表面的硫醇配体影响着团簇的催化性质, 尤其是选择性. 我们采用在真空条件下通过程序升温的方法逐渐剥除金团簇表面的硫醇配体来制备催化剂, 利用透射电镜, 红外光谱对催化剂结构进行表征, 以硝基化合物催化还原反应为模型反应, 详细研究了配体对催化活性和选择性的影响. 研究发现因配体被剥离导致底物更容易接近团簇表面, 最终使得反应转换率大幅升高. 实验结果还表明金团簇催化剂催化不同官能团取代的底物显示了良好的官能团兼容性, 有吸电子效应的硫配体使团簇表面带正电荷, 进而避免苯胺衍生物的产生.

关键词: 配体效应; 选择性; 金团簇; 催化; 纳米